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IN THE SPECIFICATION

Please make the following amendments to page 5, the 5th paragraph:

In a preferred embodiment, the method according to the invention combines a degasification of the wastes in a vacuum with a chemical reaction of the escaping gasses in a suspension of a finely ground mineral mass. Unexpectedly, the following surprising effect has been found: if the atmospheric pressure in a container filled with fresh or fermented manure of liquid muck is reduced with simultaneous moderate heating to 40 to 90 °C, then first carbon dioxide, and at a slightly higher temperature ammonia will escape from the liquid, without being accompanied by appreciable amounts of water. When these gassesgases are conducted into a suspension of a finely ground mineral mass containing calcium compounds, they will react under generation of lime and ammonium salts, but in a way that the underpressure is maintained, and the reaction is autogenously continued, if the temperature in the discharge container is maintained at the predetermined level.

Page 6, 1st paragraph, please make the following amendment:

In this way, the ammonium nitrogen <u>e. g. from a fermented manure</u> can nearly fully be removed, <u>e.g. from a fermented manure</u>. A virtually odorless sludge liquor is left, which does not gas anymore, but still contains the mineral components of the manure, such as potassium and phosphate, in the form of its compounds. From the stirred suspension in the collector, the ready-to-use nitrogen fertilizer containing lime in addition to ammonium salts, can be taken out as a concentrated suspension. It can be used without any further re-treatment.

Page 10, 3rd paragraph, please amend as follows:

After reaching the operating temperature, a pressure of 400 mbar40 kPa is adjusted in the whole system by a controlled vacuum pump (4), and the pressure reduction is performed slowly and steadily. When this pressure has been obtained, the circulation fan (6) is set into operation, so that the stripping gas is sucked-off with a defined gas throughput from the stripping container (1)

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through the line (12), and return gas from the collection container (2) is fed to the stripping process through the line (13), and by means of the ball valves 20 to 22, three preferred variants of the circulation gas flow according to the invention can be selected:

Page 11, 3rd paragraph, please amend as follows:

During the batch process, temperature and pressure in the stripping container (1) are held at approx. 80 $^{\circ}$ C and 400 to 500 mbar40 to 50 kPa by switching the heating water pump (5) or the vacuum pump (4) on and off.